

# CHE 318 Lecture 08

## Steady State Mass Transfer: More Examples

Dr. Tian Tian

2026-01-21

### Recap

- Mass transfer equations in other geometries
  - Use M.B. for  $\bar{N}_A$ , not  $N_A$
  - Be careful with the coordinate system (sphere? cylinder?)
- Solving examples with pseudo steady state assumption

### Learning Outcomes

(Continue from Lecture 07) After today's lecture, you will be able to:

- **Solve** P.S.S problems in spherical coordinates
- **Recall** difference between steady and unsteady state solutions
- **Analyze** time-dependent concentration profiles for U.S.S situations.

### P.S.S Examples (continued)

#### Example 1: Diffusion Through Stagnant B with Changing Path Length

*Adapted from Geankoplis 6.2-3*

Water vapor diffuses through a stagnant gas in a narrow vertical tube, dry air is constantly blown at the top of tube.

At time  $t$ , the liquid level is a distance  $z$  from the tube top (i.e., the diffusion path length is  $z$ ). As diffusion proceeds, the liquid level drops slowly, so  $z$  increases with time. The liquid has density  $\rho_A$ , and molecular weight  $M_A$

- Derive an expression for the time  $t_F$  required for the level to drop such that the diffusion path length changes from  $z = z_0$  at  $t = 0$  to  $z = z_F$  at  $t = t_F$ .

### Example 1: solutions



Tip

- Use pseudo steady-state assumption
- $N_A$  change over time!

Answer

$$t_F = \frac{\rho_A(z_F^2 - z_0^2)RTp_{Bm}}{2D_{AB}M_Ap_T} \frac{1}{(p_{A1} - p_{A2})}$$

### Example 2: Determine $D_{AB}$ Through Evaporation

Adapted from Griskey 10-2

Sample setup as example 4, a vertical tube of diameter  $D = 0.01128$  m contains a liquid volatile species  $A$  (chloropicrin,  $CCl_3NO_2$ ) evaporating into stagnant air ( $B$ ) at 1 atm. The gas-phase diffusion of  $A$  occurs through the air column above the liquid surface.

At  $t = 0$ , the distance from the tube top to the liquid surface is  $z_0 = 0.0388$  m, after  $t = 1$  day, the distance is  $z_1 = 0.0412$  m.

- Vapor pressure at the interface:  $p_{A1} = 3178.3$  Pa
- Liquid density:  $\rho_A = 1650$  kg/m<sup>3</sup>
- Molecular weight:  $M_A = 164.39$  kg/kmol

- Use your expression from example 4, determine the binary diffusivity  $D_{AB}$  of  $A$  in air.

### Example 2: solutions



Tip

Pseudo steady state solution and assuming  $N_A = \text{const}$  solution differ very little. Why?

Answer:

- Pseudo-steady state:  $D_{AB} = 8.56 \times 10^{-6}$  m<sup>2</sup>/s
- $N_A$  constant:  $D_{AB} = 8.75 \times 10^{-6}$  m<sup>2</sup>/s (+2.2% error)

### Example 3: P.S.S For Diffusion Through Sphere

Adapted from Geankoplis Ex 6.2-4

A sphere of naphthalene having a radius of 2.0 mm is suspended in a large volume of still air at 318 K and  $1.01325 \times 10^5$  Pa (1 atm). The surface temperature of the naphthalene can be assumed to be at 318 K and its vapor pressure at 318 K is 0.555 mm Hg. The  $D_{AB}$  of naphthalene in air at 318 K is  $6.92 \times 10^{-6}$  m<sup>2</sup>/s.

1. Calculate the rate of evaporation of naphthalene from the surface.
2. Write the expression for the time  $t_F$  to evaporate a sphere from radius  $r_0$  to  $r_F$ . The solid density for naphthalene is  $\rho$  and molecular weight is  $M_A$ .
3. What is the  $t_F$  value when the sphere is completely evaporated?

### Example 3: solutions



Tip

Similar setup as example 5.  $N_A$  is time-dependent

Answer:

1)  $N_A = 9.68 \times 10^{-8}$  kg mol/m<sup>2</sup>/s

2) Expression for  $t_F r = r_F$ :

$$t_F(r = r_F) = \frac{\rho R T p_{Bm}}{2 M_A D_{AB} p_T} \frac{1}{(p_{A1} - p_{A2})} (r_0^2 - r_F^2)$$

3) Expression for  $t_F(r = 0)$ :

$$t_F(r = 0) = \frac{\rho R T p_{Bm} r_0^2}{2 M_A D_{AB} p_T} \frac{1}{(p_{A1} - p_{A2})}$$

Compare the solutions with Example 4. We can also measure the diffusivity of volatile organic molecules using the sphere evaporation method!

### Summary

- Pseudo-steady state solutions to diffusion-evaporation problems
- We will discuss about unsteady state mass transfer next lecture!