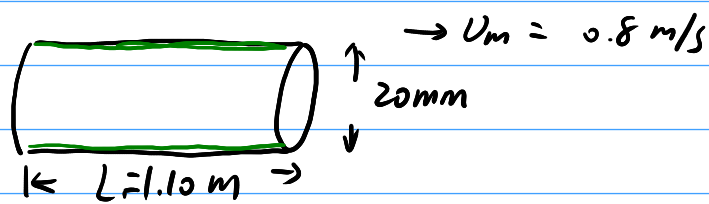


CHE 318 L19

Dimensionless number examples

Case 1



$$D_{AB} = 6.92 \times 10^{-6} \text{ m}^2/\text{s} \quad P_{Ai} = 74.0 \text{ Pa} \quad \left\{ \begin{array}{l} \mu = 1.932 \times 10^{-5} \text{ Pa} \cdot \text{s} \\ \rho = 1.114 \text{ kg/m}^3 \end{array} \right.$$

Gas!

$$1) \quad N_{Re} = \frac{D \cdot U_m \cdot \rho}{\mu} = \frac{0.020 \times 0.80 \times 1.114}{1.932 \times 10^{-5}} = 922.6$$

$$N_{Sc} = \frac{\mu}{\rho D_{AB}} = \frac{1.932 \times 10^{-5}}{1.114 \times 6.92 \times 10^{-6}} = 2.506$$

Laminar gas flow. Need to use "rod-like"

$$\begin{aligned} \text{x-axis} \quad \frac{W}{D_{AB} \cdot \rho \cdot L} &= N_{Re} \cdot N_{Sc} \cdot \frac{D}{L} \cdot \frac{\pi}{4} \\ &= 922.6 \times 2.506 \times \frac{0.020}{1.10} \cdot \frac{3.1416}{4} = 33.02 \end{aligned}$$

$$\begin{aligned} \text{How to get } W? \quad W &= \frac{[\text{kg}]}{[\text{s}]} = \rho \cdot v \cdot A_{\text{tube}} = \rho \cdot U_m \cdot \frac{\pi D^2}{4} \\ &= 1.114 \times 0.80 \times 3.1416 \times (0.020)^2 / 4 \\ &= 2.80 \times 10^{-4} \text{ kg/s} \end{aligned}$$

(the same if use $W = 33.02 \times \rho \times D_{AB} \times L$)

$$\begin{aligned} \text{Use plot, } \left\{ \begin{array}{l} \text{x-axis} = 33.02 \\ \text{y-axis} = 0.55 \end{array} \right. & \quad \frac{C_A - C_{A0} \Rightarrow 0}{C_{Ai} - C_{A0} = 0} = 0.55 \end{aligned}$$

$$C_A = C_{Ai} \cdot 0.55 = 2.799 \times 10^5 \times 0.55 = 1.539 \times 10^5 \text{ kg mol/m}^3$$

$$C_{Ai} = P_{Ai} / RT = 74.0 / 8314 / 318 = 2.799 \times 10^5 \text{ kg mol/m}^3$$

2) How will result change if we double U ?

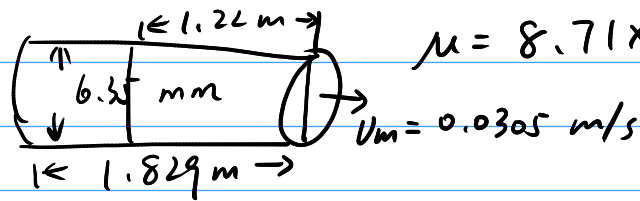
$$x\text{-axis } N_{Re} N_{Sc} \frac{D}{L} \frac{\pi}{4} \propto U_m$$

$$U_m' = 2 \times U_m \Rightarrow x\text{-axis becomes doubled}$$

search $x \rightarrow$ axis \rightarrow y -axis, read out C_A

3) If $D_{AB} \downarrow \frac{W}{D_{AB} P L} \uparrow \Rightarrow$ Lower outlet conc \checkmark

Case 1-2 $T = 28,1^\circ\text{C}$ $\rho = 996 \text{ kg/m}^3$



$$\mu = 8.71 \times 10^{-4} \text{ Pa}\cdot\text{s}$$

$$C_{A,i} = 0.02948 \text{ kg mol/m}^3 \quad D_{AB} (\text{liq}) = 1.245 \times 10^{-9} \text{ m}^2/\text{s}$$

C_A at outlet?

Please use the cheatsheet!

$$1) N_{Re} = \frac{L_0 \cdot v_m \cdot \rho}{\mu} = \frac{0.00635 \times 0.0305 \times 996}{8.71 \times 10^{-4}} = 221.4$$

It's laminar flow

$$N_{Sc} = \frac{\mu}{\rho D_{AB}} = \frac{8.71 \times 10^{-4}}{996 \times 1.245 \times 10^{-9}} = 702.41$$

$$W = \rho \cdot v_m \cdot \frac{\pi D^2}{4} = 996 \times 0.0305 \times \frac{3.1416 \times (6.35 \times 10^{-3})^2}{4} = 9.616 \times 10^{-4} \text{ kg/s}$$

$$x\text{-axis} \quad N_{Re} \cdot N_{Sc} \cdot \frac{D}{L} \cdot \frac{\pi}{4} = 634.4$$

↑
use 1.22 m, not 1.829 m!

x -axis > 400 , follow the parabolic line

$$\frac{C_A - C_{A0}}{C_{A,i} - C_{A0}} = \frac{C_A - 0}{0.02948 - 0} = 5.5 \times 634.4^{-\frac{2}{3}}$$

$$C_A = 2.196 \times 10^{-3} \text{ kg mol/m}^3$$