

# CHE 318 Lecture 28

## Humidification Process II

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### Learning outcomes

After this lecture, you will be able to:

- **Recall** humidification and cooling paths on the psychrometric chart.
- **Describe** the origin of wet-bulb temperature and latent-heat effects during evaporation.
- **Analyze** adiabatic saturation using coupled heat and mass balances.
- **Apply** the psychrometric chart to obtain humidity-related properties.

# Cheatsheet for humidification process

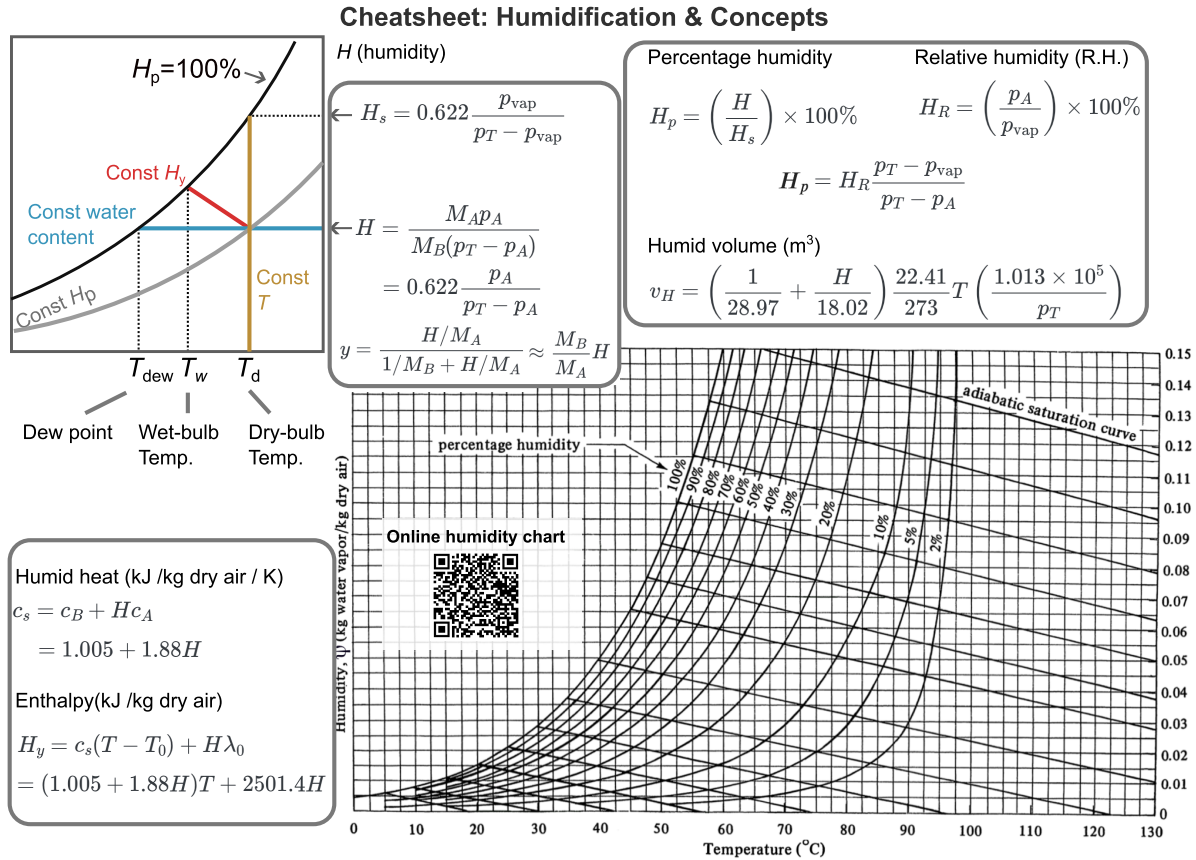


Figure 1: Charts distributed in class.

## Reading the humidity / psychrometric chart (level 1)

Find where  $H$ ,  $H_p$ , dew point  $T_{dew}$  are?

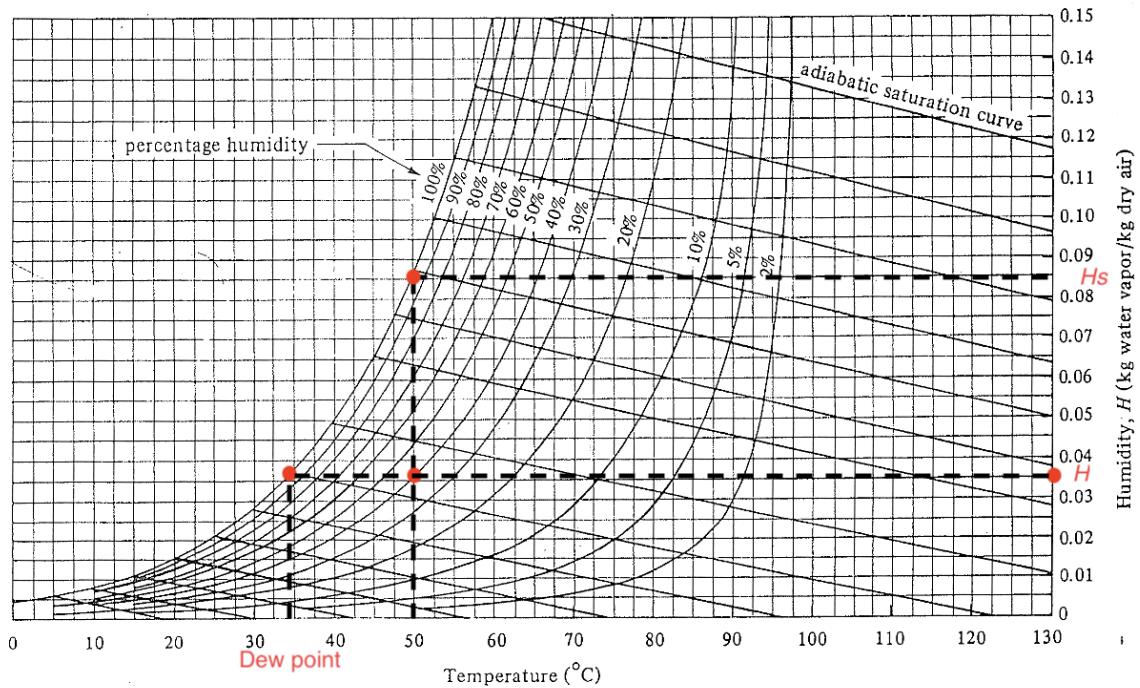


FIGURE 9.3-2. Humidity chart for mixtures of air and water vapor at a total pressure of 101.325 kPa (760 mm Hg). (From R. E. Treybal, *Mass-Transfer Operations*, 3rd ed. New York: McGraw-Hill Book Company, 1980. With permission.)

### Example 2: humidifier design

A living room of 60 m<sup>2</sup> at 22 °C has a relative humidity of 20% due to continuous heating. You and your roommate wish to purchase a humidifier that can humidify the living room up to 45% relative humidity. Assume the floor-ceiling distance is 3 m, calculate the weight of water needed to humidify the whole room. Can you use the humidity chart to estimate?

### Example 2: steps

1. Read the saturation vapour pressure from  $H_s$  ( $H_s = 0.017$ )

$$H_s = 0.622 \frac{p_{\text{vap}}}{p_T - p_{\text{vap}}} = 0.017 \quad (1)$$

$$p_{\text{vap}} = 2.69 \text{ kPa} \quad (2)$$

from the vapour data it gets  $p_{\text{vap}} = 2.64 \text{ kPa}$ , pretty close!

2. Estimate weight of water  $\Delta m_A$

$$\Delta m_A = \frac{\Delta p_A V M_A}{RT} \quad (3)$$

$$= \frac{(H_{R1} - H_{R0}) p_{\text{vap}} V M_A}{RT} \quad (4)$$

$$\approx 0.87 \text{ kg} \quad (5)$$

Does it make sense? The requirement for water tank will be a lower bound.

### Mythbusting time (1)

My weather app shows that outside is  $-12^\circ\text{C}$  and R.H. is 74%, where the dew point is  $-16^\circ\text{C}$ . What does all that mean?

#### Tip

A useful note is that the **lower** dew point is compared with current temperature, the **drier** air appears to be

### Mythbusting time (2)

In the previous scenario  $-12^\circ\text{C}$  and R.H. is 74%, when I open the door, my humidity in home immediately drops! Why?

- The calculated  $H_R$  at room temperature is only 6.7% if fully filled with outside air.

#### Tip

$H_R$  (or R.H.) only measures up at current temperature. When moving water content at different  $T$ ,  $H_R$  will change.

- cold air appears to be dry at high  $T$
- warm air appears to be humid at low  $T$

### Mythbusting time (3)

Why does “humid hot” environment feels much hotter than “dry hot” environment, even if the apparent  $T$  is the same?

- Calculate the enthalpy of air-water mixture,  $H_y$  significantly increases when relative humidity is high!
- Human body relies on cooling to survive. At high  $T$  high  $H_R$ , both driving forces for evaporation are reduced:
  - $T_{\text{body}} - T_{\text{env}}$  becomes small bad dissipation
  - $p_{A,\text{body}} - p_{A,\text{env}}$  becomes small evaporation suppressed

#### Tip

The sensible specific heat for air-water mixture does not change significantly, even if water vapour's heat capacity is higher. (absolute  $H$  is always 0.1 when  $T < 50$  °C)

### Measuring humidity: the two-bulb hygrometer

Before electronic sensors, humidity was measured using a **two-thermometer setup**

- One thermometer measures **dry-bulb temperature**  $T_d$
- The second thermometer is wrapped with a **wet wick** and measures **wet-bulb temperature**  $T_w$  ( $T_w < T_d$ )

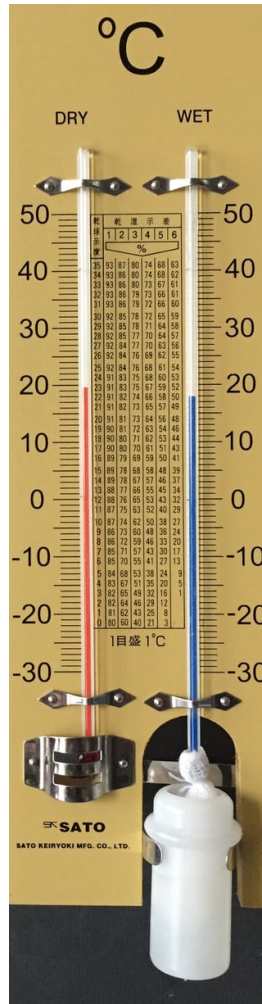


Figure 2: Two-bulb hygrometer

### What does the wet bulb tell us?

The wet bulb is a **steady state** evaporative cooling experiment, which can be generalized for interfacial evaporation problem:

- In and outlet temperatures are the same, while outlet humidity is higher
- Evaporation consumes **latent heat**

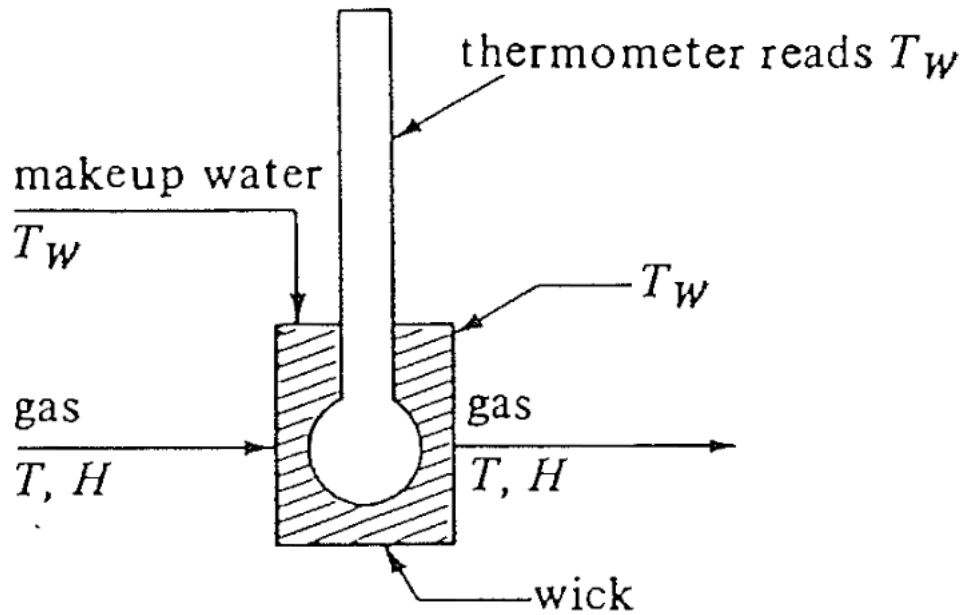


FIGURE 9.3-4. *Measurement of wet bulb temperature.*

### Concept of wet-bulb temperature

- The wet-bulb temperature  $T_w$  is the temperature reached by a **wet surface exposed to air**

$$T_w < T_d$$

- $T_d$  = dry-bulb temperature
- $T_w$  = wet-bulb temperature
- The difference between  $T_w$  and  $T_d$  indicates the inlet air humidity

### Moist air enthalpy

From [Lecture 27](#), the specific enthalpy of moist air can be written as

$$H_y = (1.005 + 1.88H)(T - T_0) + 2501.4H \quad (6)$$

- Increase the absolute humidity  $H$  must cause  $H_y$  to increase gas phase takes heat from liquid.
- Solving the heat + mass balance will give solution to  $T_w$ .

### Heat balance around the wet bulb

Consider the control volume around the wet bulb. Heat transferred from the air is used to evaporate water, linked by the heat-mass balance (need a bit prerequisite in heat transfer):

$$q = M_A \lambda_w A N_A \quad (7)$$

- $m_A$ : molecular weight of water
- $\lambda_w$ : latent heat of vaporization at  $T_w$  (44045 kJ/kg mol at 1 atm)
- $A$ : area of the wetted surface
- $N_A$ : molar flux of evaporating water

### R.H.S.: mass transfer at the interface

The evaporation rate can be written as

$$N_A = k_y (y_w - y) \quad (8)$$

- $k_y$ : gas-phase mass transfer coefficient (since  $y_{BM} \approx 1$ ,  $k_y \approx k'_y$ )
- $y_w$ : vapor mole fraction at the interface (saturated at  $T_w$ )
- $y$ : vapor mole fraction in bulk air

### Converting humidity to mole fraction

We can further change  $y$  to the humidity  $H$  for dilute system. Since humidity is define as weight ratio:

$$H = \frac{\text{kg } H_2O}{\text{kg dry air}} \quad (9)$$

The mole fraction of vapor is

$$y = \frac{H/M_A}{1/M_B + H/M_A} \quad (10)$$

Since humidity is typically small

$$y \approx \frac{M_B}{M_A} H \quad (11)$$

### **L.H.S. heat transfer to the wet surface**

The heat flux  $q$  in L.H.S. from the air to the wet surface is

$$q = h(T - T_w)A \quad (12)$$

where  $h$  is heat transfer coefficient in the Fourier's law  $q = -h\Delta T$

### **Wet-bulb setup: final results**

Combining heat transfer ( $q$ ) and mass transfer ( $N_A$ ) relations gives

$$\frac{H - H_w}{T - T_w} = -\frac{h}{M_B k_y \lambda_w} \quad (13)$$

Note  $\frac{H - H_w}{T - T_w}$  means the slope of a line on the psychrometric chart. The slope is almost identical to **adiabatic line!**

## Psychrometric chart: adiabatic line (level 2)

The  $(T_d, H_{in})$  and  $(T_w, H_{out})$  points are along the adiabatic line (no external heat exchange). For water-air system, the adiabatic line and cooling line are very close and often not distinguished.

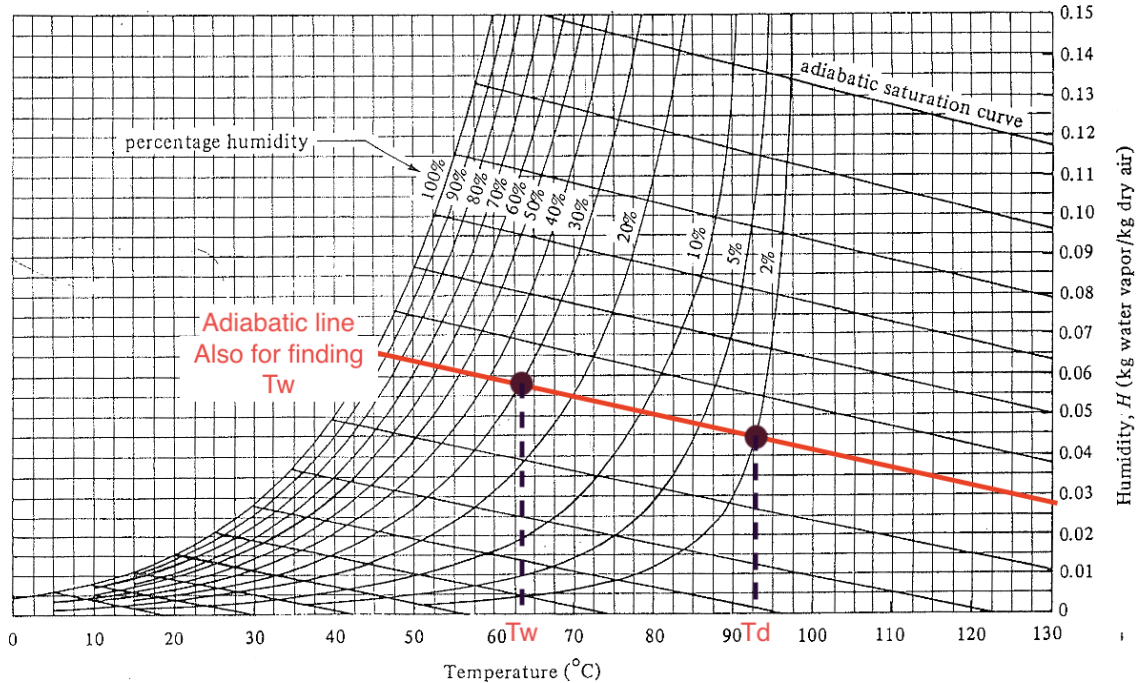


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## Deeper look into the cooling process (1)

What does the adiabatic line tell us? It is basically a process that each point has the same humid enthalpy, and no change of heat to external system:

$$H = c_s(T - T_0) + H\lambda_0 = [\text{Const}]$$

- Increase humidity decrease  $T$
- Lowest temperature can reach in the system at certain  $H_{out}$  is  $T_w$
- Lowest temperature can reach when air is saturated is  $T_s$

## Deeper look into the cooling process (2)

For water-air, one handy property is that

$$\frac{h}{M_B k_y} \approx 1.005 \approx c_s \quad [\text{kJ} / \text{kg air}]$$

such relation allows us to use the humidity chart's adiabatic saturation curve.

### Warning

Such simplification may not be applicable for other liquid, such as benzene!

## What to learn next

The wet-bulb experiment connects **heat transfer** and **mass transfer**, and the evaporation rate depends on the **vapor pressure driving force**.

Next topics we will study:

- Gas-phase mass transfer during evaporation
- Interfacial equilibrium between water and air
- Driving force expressed as  $(y_w - y)$  or  $(p_{sat} - p_A)$

## Summary

- Reading humidity chart for cooling process
- Wet-bulb temperature and its origin
- Calculation of humidity values from the chart + equation